

KDC-6 – For optimal methylamine productivity during your catalyst life cycle

Albemarle KDC-6 catalyst is the state-of-the-art commercial choice used in many methylamine production units around the world. Compared with its predecessors, KDC-6 offers superior activity, stability, strength and overall productivity. Low carbon formation on the catalyst prevents particle swelling, which, combined with the catalyst's high initial strength, means that slow pressure drop build-up over time during the catalyst cycle is not seen. This gives KDC-6 its long cycle time and high productivity over the run.

Methylamine production

The reaction of ammonia and methanol in the presence of a solid acid catalyst forms a mixture of mono-, di- and trimethylamine (MMA, DMA and TMA, respectively). They are important intermediates in the manufacture of various industrial chemicals. The major outlets for the respective amines include

- **MMA:** chemicals (n-methyl-2-pyrrolidone and n-methyl-diethanolamine), pesticides and explosives
- **DMA:** chemicals (dimethylformamide and dimethylacetamide), water treatment chemicals and detergents
- **TMA:** animal food additives (choline chloride).

Globally, the demand for the different methylamines shows large regional variations. For instance, in Europe the consumption ratio of

MMA:DMA:TMA is 1:3:1, whereas in Asia the ratio can be 1:8:1. This ratio is subject to change owing to the increasing number of outlets for MMA, for example, n-methyl-2-pyrrolidone, a solvent.

Methylamines are synthesized from methanol and excess ammonia in a gas-phase reaction at 300–500°C and at elevated pressure in the presence of a solid acid catalyst to form an equilibrium mixture of roughly 25:30:45 MMA:DMA:TMA. With the market favoring DMA production, large quantities of MMA and TMA have to be recycled to maximize the production of DMA. This is the basis for the well-known Leonard process, a schematic for which is shown in Figure 1.

In the Leonard process, fresh methanol and ammonia feed are combined with recycled ammonia and methylamines (mainly MMA and TMA) and are fed to a reactor containing a solid acid catalyst. The amorphous silica alumina catalysts produced by Albemarle are those most commonly used in the methylamine production process. These catalysts are highly active and stable but have no specific product selectivity. Therefore, the equilibrium mixture of MMA, DMA and TMA is obtained, provided the process conditions are optimized. The mixture is then purified to a high level (see Figure 1). In modern set-ups, a methanol recovery facility can also be added.

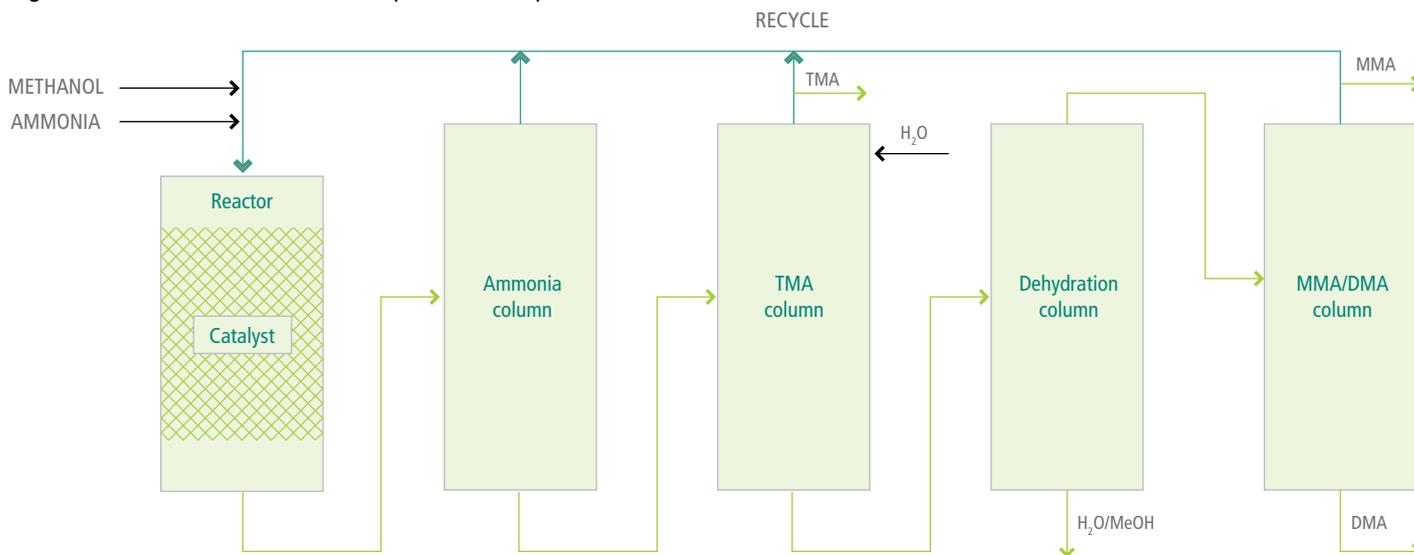


Figure 1: Process schematic for methylamine production.

Catalysts for methylamine production

Currently, all the catalysts used for methylamine production yield the equilibrium composition of methylamines. Zeolites with narrow pores show enhanced selectivity for DMA. However, they have lower activity and stability than amorphous catalysts. The Nitto process for production of MMA and DMA is based on technology using zeolites. However, sizeable quantities of TMA are formed and therefore this process requires an amorphous silica alumina catalyst (in a separate reactor) to disproportionate TMA.

Historically, Albemarle has continuously improved the activity and stability of its catalysts for methylamine production, and now KDC-6 catalyst is widely applied in methylamine production units around the world. Figure 2 shows the historical development of the activity of various Albemarle methylamine catalysts. Table 1 shows the typical productivities and lives of some of the catalysts.



Figure 2: Activity levels of successive generations of Albemarle methylamine catalysts.

	LA-30	KDC-4	KDC-6
Productivity, ton methanol/ton catalyst	3,500–5,000	5,000–8,000	10,000–15,000
Life, months	8–12	12–28	18–36

Table 1: Productivity (typical range, depending on conditions) and life of successive Albemarle catalyst generations.

Typical product properties	↘
Catalyst name	KDC-6
Application	Methylamine production
SiO ₂ , %db	21
Al ₂ O ₃ , %db	Balance
Size, mm	5
Shape	Pellet
Estimated reactor density, kg/m ³	470–520
Surface area, m ² /g	350
Average side crushing strength, lb	Minimum 30
Packaging	210-L drum, 100 kg per drum

↘ For more information on this or other Albemarle products and technologies, please contact your Albemarle representative.

AMERICAS

2625 Bay Area Blvd
Suite 250
Houston, TX 77058
USA

Tel: +1 281 480 4747
Email: catmaster@albemarle.com

EUROPE AND AFRICA

Nieuwendammerkade 1–3
1030 BE Amsterdam
The Netherlands

Tel: +31 20 634 7300
Email: catmaster@albemarle.com

MIDDLE EAST AND INDIA

PO Box 293774
6W Block A, Office 512
Dubai Airport Free Zone
Dubai

Tel: +971 4 701 7770
Email: catmaster@albemarle.com

ASIA PACIFIC

Room 2208, Shui On Plaza
No. 333 Huai Hai Zhong Rd
Shanghai 200021
China

Tel: +86 21 6103 8666
Email: catmaster@albemarle.com

www.albemarle.com

The information presented herein is believed to be accurate and reliable, but is presented without guarantee or responsibility on the part of Albemarle Corporation. It is the responsibility of the user to comply with all applicable laws and regulations and to provide for a safe workplace. The user should consider any information contained herein, including information about any health or safety hazards, only as a guide, and should take those precautions that are necessary or prudent to instruct employees and to develop work practice procedures in order to promote a safe work environment. Further, nothing contained herein shall be taken as an inducement or recommendation to manufacture or use any of the herein described materials or processes in violation of existing or future patents.

© 2011 Albemarle Corporation. All rights reserved worldwide.

Cat-221469-0411.